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Applicant: Exxon Research and Engineering Company
P.O.Box 390 180 Park Avenue
Florham Park New Jersey 07932(US)

72

Inventor: Ewen, John Alexander
16615 Kentwood
Houston Texas(US)

72

Inventor: Welborn, Howard Curtis, Jr.
1502 Driscoll Street
Houston Texas(US)

74

Representative: Northover, Robert Frank et al,
ESSO Chemical Limited Esso Chemical Research Centre
P.O. Box 1
Abingdon Oxfordshire, OX13 6BB(GB)

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Process and catalyst for producing poly-ethylene having a broad molecular weight distribution.

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Polyolefins having a broad molecular weight distribution are obtained by polymerizing ethylene or higher alpha-olefins in the presence of a catalyst system comprising two or more metallocenes each having different propagation and termination rate constants and alumoxane.

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**PROCESS AND CATALYST FOR PRODUCING POLYETHYLENE HAVING
A BROAD MOLECULAR WEIGHT DISTRIBUTION**

1 The present invention concerns catalyst and process for the
2 polymerization of ethylene. More particularly, the invention
3 relates to catalysts and process for the polymerization of
4 ethylene to polyethylene having a broad or multimodal molecular
5 weight distribution.

6 It is known that certain metallocenes such as
7 bis(cyclopentadienyl) titanium or zirconium dialkyls in
8 combination with aluminum alkyl co-catalyst, form homogeneous
9 catalyst systems useful for the polymerization of ethylene.
10 German Patent Application 2,608,863 discloses the use of a
11 catalyst system for the polymerization of ethylene consisting
12 of bis(cyclopentadienyl)titanium dialkyl, aluminum trialkyl and
13 water. German Patent Application 2,608,933 discloses an
14 ethylene polymerization catalyst system consisting of zirconium
15 metallocenes of the general formula
16 $(\text{cyclopentadienyl})_n\text{ZrY}_{4-n}$, wherein n stands for a number in
17 the range of 1 to 4, Y for R, CH_2AlR_2 , $\text{CH}_2\text{CH}_2\text{AlR}_2$ and
18 $\text{CH}_2\text{CH}(\text{AlR}_2)_2$ wherein R stands for alkyl or metallo alkyl;
19 an aluminum trialkyl cocatalyst and water.

20 European Patent Appln. No. 0035242 discloses a process for
21 preparing ethylene and atactic propylene polymers in the
22 presence of a halogen-free Ziegler catalyst system of (1) a
23 cyclopentadienyl compound of the formula
24 $(\text{cyclopentadienyl})_n\text{MeY}_{4-n}$ in which n is an integer from 1
25 to 4, Me is a transition metal, especially zirconium, and Y is
26 either hydrogen, a $\text{C}_1\text{-C}_5$ alkyl or metallo alkyl group or a
27 group of the general formula CH_2AlR_2 , $\text{CH}_2\text{CH}_2\text{AlR}_2$ and
28 $\text{CH}_2\text{CH}(\text{AlR}_2)_2$ in which R represents a $\text{C}_1\text{-C}_5$ alkyl or
29 metallo alkyl group, and (2) an alumoxane.

30 The above disclosures demonstrate the usefulness of certain
31 specific metallocenes in combination with certain aluminum
32 compounds for the polymerization of ethylene and particularly
33 polymerization at a high activity. The above described
34 catalysts comprising titanium and zirconium metallocenes being
35 homogeneous, produce polyethylenes of narrow molecular weight
36 distribution (MWD) i.e. \bar{M}_w/\bar{M}_n of from 2-4. Hence, the

1 references neither disclose polyethylenes having a broad
2 molecular weight distribution and/or a multimodal molecular
3 weight distribution, nor how to obtain such polyethylenes.

4 U. S. Patent 4,310,648 discloses a catalytic reaction
5 product of a titanium compound, a zirconium compound, an
6 organomagnesium compound and a halide source. The reaction
7 product (a heterogeneous catalyst) when employed in combination
8 with aluminum alkyls is useful for the production at high
9 activity of broad molecular weight polyethylenes.

10 U. S. Patent 4,361,685 discloses the use of organic soluble
11 chromium and zirconium compounds to be employed in combination
12 with a supported catalyst system comprising an organometallic
13 activating agent and a trivalent or tetravalent titanium
14 compound. The polymers obtained have a high molecular weight
15 and a narrow molecular weight distribution.

16 In "Molecular Weight Distribution And Stereoregularity Of
17 Polypropylenes Obtained With
18 $Ti(OC_4H_9)_4/Al_2(C_2H_3)_3$ Catalyst System"; Polymer,
19 Pg. 469-471, 1981, Vol. 22, April, Doi, et al disclose
20 propylene polymerization with a catalyst which at about $41^{\circ}C$
21 obtains a soluble catalyst and insoluble catalyst fraction, one
22 with "homogeneous catalytic centres" and the other with
23 "heterogeneous catalytic centres". The polymerization at that
24 temperature obtains polypropylene having a bimodal molecular
25 weight distribution.

26 It is highly desirable to have for many application, such
27 as an extrusion and molding processes, polyethylenes which have
28 a broad molecular weight distribution of the unimodal and/or
29 the multimodal type. Such polyethylenes evidence excellent
30 processability, i.e., they can be processed at a faster
31 throughput rate with lower energy requirements and at the same
32 time such polymers would evidence reduced melt flow
33 perturbations.

34 In view of the foregoing problems, it would be highly
35 desirable to provide a polymerization catalyst system of high
36 activity to produce high quality ethylene polymers which

evidence broad molecular weight distribution. It is furthermore highly desirable to be able to produce the ethylene polymers directly in a single reactor, i.e., without having to blend polyethylenes having different molecular weights and distributions in order to obtain the advantages of this invention.

SUMMARY OF THE INVENTION

The present invention provides polyethylene having a broad molecular weight and/or a multimodal molecular weight distribution. The polyethylenes are obtained directly from a single polymerization process, i.e., the polyethylenes of this invention are obtained without requiring blending techniques. The invention furthermore provides a catalyst system for the polymerization of ethylene directly to polyethylene having a broad molecular weight distribution especially a multimodal molecular weight distribution, and particularly a bimodal MWD. The invention further provides a process for polymerizing ethylene in the presence of the catalyst system.

Accordingly, there is provided catalyst systems and especially systems for the polymerization of ethylene to polyethylene having a broad molecular weight distribution and especially a bimodal or multimodal molecular weight distribution; said catalyst system comprising (a) at least two different metallocenes each having different propagation and termination rate constants for ethylene polymerizations and (b) an alumoxane. The metallocenes employed in accordance with this invention are organometallic coordination compounds which are cyclopentadienyl derivatives of a transition metal of Group 4b, 5b and 6b metals of the Periodic Table and include mono, di and tricyclopentadienyls and their derivatives of the transition metals. The metallocenes can be represented by the general formula $(C_5R'_m)_pR''_s(C_5R'_m)_2MeQ_{3-p}$ or $R''_s(C_5R'_m)MeQ'$, wherein $(C_5R'_m)$ is a cyclopentadienyl or substituted cyclopentadienyl, each R' , which can be the same

1 or different, is hydrogen or a hydrocarbyl radical such as
2 alkyl, alkenyl, aryl, alkylaryl, or arylalkyl radical having
3 from 1 to 20 carbon atoms or two carbon atoms of the
4 cyclopentadienyl ring are joined together to form a C_4-C_6
5 ring, R'' is a C_1-C_4 alkylene radical, a dialkyl germanium
6 or silicone or an alkyl phosphine or amine radical bridging two
7 $(C_5R'_m)$ rings, Q is a hydrocarbon radical such as aryl,
8 alkyl, alkenyl, alkylaryl, or arylalkyl radical having from 1
9 to 20 carbon atoms or halogen and can be the same or different,
10 Q' is an alkylidene radical having from 1 to 20 carbon
11 atoms, Me is a Group 4b, 5b and 6b metal of the Periodic Table
12 (Chemical Rubber Company's Handbook of Chemistry and Physics,
13 48th Edition), s is 0 or 1, p is 0, 1 or 2; when $p = 0$, $s = 0$;
14 m is 4 when s is 1 and m is 5 when s is 0.

15 The present invention also provides a process for producing
16 polyethylenes having a high molecular weight as well as a broad
17 molecular weight distribution and especially MWD of the bimodal
18 type. The process comprises polymerizing ethylene
19 alone or ethylene with minor amounts of higher alpha-olefins in
20 the presence of the homogeneous catalyst system described above.

21 The present invention furthermore provides high molecular
22 weight polyethylene having a bimodal molecular weight
23 distribution.

24 It is highly surprising that two different metallocenes in
25 combination with an alumoxane can produce polyethylene having a
26 broad MWD since the individual metallocenes with an alumoxane
27 generally obtains polyethylene having a narrow MWD. In
28 accordance with this invention, however, one can advantageously
29 tailor polyethylene having desired molecular weights and
30 molecular weight distributions by the judicious selection of
31 metallocenes.

32 BRIEF DESCRIPTION OF THE FIGURES

33 Figure 1 is a plot of the molecular weight distribution of
34 polyethylene prepared as in Example 1 and in accordance with
35 this invention.

1 Figure 2 is a plot of the molecular weight distribution of
2 polyethylene prepared as in comparative example 1B showing a
3 narrow unimodal MWD.

4 Figure 3 is a plot of the molecular weight distribution of
5 polyethylene prepared as in comparative example 1A showing a
6 narrow unimodal MWD.

7 Figure 4 is a plot of the molecular weight distribution of
8 polyethylene prepared as in example 2 and showing a bimodal MWD.

9 Figure 5 is a plot of the molecular weight distribution of
10 polyethylene prepared as in example 3 showing a bimodal MWD.

11 DETAILED DESCRIPTION OF THE INVENTION

12 The present invention is directed towards a catalytic
13 process for the polymerization of ethylene to high molecular
14 weight polyethylenes evidencing a broad and/or multimodal
15 molecular weight distribution. The polymers are intended for
16 fabrication into articles by extrusion, injection molding,
17 thermoforming, rotational molding, and the like. In
18 particular, the polymers of this invention are homopolymers of
19 ethylene, however, minor amounts of higher alpha-olefins having
20 from 3 to 10 carbon atoms and preferably 4 to 8 carbon
21 atoms can be copolymerized with ethylene. Illustrative of the
22 higher alpha-olefins are butene-1, hexene-1 and octene-1.

23 In the process of the present invention, ethylene, either
24 alone or together with minor amounts of alpha-olefins, is
25 polymerized in the presence of a catalyst system comprising at
26 least two metallocenes and an alumoxane.

27 The alumoxanes are well known in the art and are polymeric
28 aluminum compounds which can be represented by the general
29 formulae $(R-Al-O)_n$ which is a cyclic compound and
30 $R(R-Al-O)_nAlR_2$, which is a linear compound. In the
31 general formula R is a C_1-C_5 alkyl group such as, for
32 example, methyl, ethyl, propyl, butyl and pentyl and n is an
33 integer from 1 to 20. Most preferably, R is methyl.
34 Generally, in the preparation of alumoxanes from, for example,

1 aluminum trimethyl and water, a mixture of the linear and
2 cyclic compounds are obtained.

3 The alumoxanes can be prepared in various ways.
4 Preferably, they are prepared by contacting water with a
5 solution of aluminum trialkyl, such as, for example, aluminum
6 trimethyl, in a suitable organic solvent such as benzene or an
7 aliphatic hydrocarbon. For example, the aluminum alkyl is
8 treated with water in the form of a moist solvent or the
9 aluminum alkyl such as aluminum trimethyl can be desirably
10 contacted with a hydrated salt such as hydrated copper sulfate.

11 Preferably, the alumoxane is prepared in the presence of a
12 hydrated copper sulfate. The method comprises treating a
13 dilute solution of aluminum trimethyl in, for example, toluene,
14 with copper sulfate represented by the general formula
15 $\text{CuSO}_4 \cdot 5\text{H}_2\text{O}$. The ratio of copper sulfate to aluminum
16 trimethyl is desirably about 1 mole of copper sulfate for 5
17 moles of aluminum trimethyl. The reaction is evidenced by the
18 evolution of methane.

19 The metallocenes employed each should have different
20 propagation and termination rate constants with respect to
21 ethylene polymerization. Such rate constants can be determined
22 by one of ordinary skill in the art. The metallocenes are the
23 organometallic coordination compound which are the mono, di and
24 tricyclopentadienyls and their derivatives of a transition
25 metal of Group 4b, 5b and 6b metals of the Periodic Table. The
26 more desirable metallocenes employed in accordance with the
27 invention are represented by the general formula

28 $(\text{C}_5\text{R}'_{\text{m}})_p \text{R}'' (\text{C}_5\text{R}'_{\text{m}})_q \text{MeQ}_{3-p}$ and
29 $\text{R}'' (\text{C}_5\text{R}'_{\text{m}})_2 \text{MeQ}'$ wherein $(\text{C}_5\text{R}'_{\text{m}})$ is cyclopentadienyl
30 or substituted cyclopentadienyl, each R' is the same or
31 different and is hydrogen or a hydrocarbyl radical such as
32 alkyl, alkenyl, aryl, alkylaryl, or arylalkyl radicals
33 containing from 1 to 20 carbon atoms or two adjacent carbon
34 atoms are joined together to form a $\text{C}_4\text{-C}_6$ ring, R'' is a
35 $\text{C}_1\text{-C}_4$ alkylene radical, a dialkyl germanium or silicone or
36 an alkyl phosphine or amine radical bridging two $(\text{C}_5\text{R}'_{\text{m}})$

1 rings, Q is a hydrocarbyl radical such as aryl, alkyl, alkenyl,
 2 alkylaryl, or arylalkyl radical having from 1-20 carbon atoms
 3 or halogen and can be the same or different, Q' is an
 4 alkylidene radical having from 1 to 20 carbon atoms, s is
 5 0 or 1, p is 0, 1 or 2; when p is 0, s is 0; m is 4 when s is 1
 6 and m is 5 when s is 0 and Me is a Group 4b, 5b or 6b metal of
 7 the Periodic Table.

8 Exemplary hydrocarbyl radicals are methyl, ethyl, propyl,
 9 butyl, amyl, isoamyl, hexyl, isobutyl, heptyl, octyl, nonyl,
 10 decyl, cetyl, 2-ethylhexyl, phenyl, and the like.

11 Exemplary alkylene radicals are methylene, ethylene,
 12 propylene, and the like.

13 Exemplary halogen atoms include chlorine, bromine and
 14 iodine and of these halogen atoms, chlorine is preferred.

15 Exemplary of the alkylid radicals is methylidene,
 16 ethylidene and propylidene.

17 The multiple metallocene system usefully employed in
 18 accordance with this invention are preferably the mono, bi and
 19 tricyclopentadienyl or substituted cyclopentadienyl titanium
 20 (IV) and zirconium (IV) compounds represented by the general
 21 formula.

22 Illustrative but non-limiting examples of the titanocenes
 23 which can be usefully employed in accordance with this
 24 invention are monocyclopentadienyl titanocenes, such as
 25 cyclopentadienyl titanium trichloride,

26 pentamethylcyclopentadienyl titanium trichloride;
 27 bis(cyclopentadienyl) titanium diphenyl, the carbene
 28 represented by the formula $\text{Cp}_2\text{Ti}=\text{CH}_2 \cdot \text{Al}(\text{CH}_3)_2\text{Cl}$,
 29 and derivatives of this reagent such as

30 $\text{Cp}_2\text{Ti}=\text{CH}_2 \cdot \text{Al}(\text{CH}_3)_3$, $(\text{Cp}_2\text{TiCH}_2)_2$,

31 $\text{Cp}_2\text{TiCH}_2\text{CH}(\text{CH}_3)\text{CH}_2$, $\text{Cp}_2\text{Ti}=\text{CHCH}_2\text{CH}_2$,

32 $\text{Cp}_2\text{Ti}=\text{CH}_2 \cdot \text{AlR}'''_2\text{Cl}$, wherein Cp is a cyclopentadienyl
 33 or substituted cyclopentadienyl radical, and R''' is an alkyl,
 34 aryl or alkylaryl radical having from 1-18 carbon atoms;
 35 substituted bis(Cp)Ti(IV) compounds such as bis(indenyl)Ti

1 diphenyl or dichloride, bis(methylcyclopentadienyl)Ti diphenyl
 2 or dihalides and other dihalide complexes; dialkyl, trialkyl,
 3 tetra-alkyl and penta-alkyl cyclopentadienyl titanium
 4 compounds, such as bis(1,2-dimethylcyclopentadienyl)Ti diphenyl
 5 or dichloride, bis(1,2-diethylcyclopentadienyl)Ti diphenyl or
 6 dichloride and other dihalide complexes.

7 Illustrative but non-limiting examples of the zirconocenes
 8 which can be usefully employed in accordance with this
 9 invention are monocyclopentadienyl zirconocenes, such as
 10 cyclopentadienyl zirconium trichloride, pentamethyl
 11 cyclopentadienyl zirconium trichloride;
 12 bis(cyclopentadienyl)zirconium diphenyl,
 13 bis(cyclopentadienyl)zirconium dimethyl, the alkyl substituted
 14 cyclopentadienes, such as bis(ethyl cyclopentadienyl)zirconium
 15 dimethyl, bis(β -phenylpropylcyclopentadienyl)zirconium
 16 dimethyl, bis(methylcyclopentadienyl)zirconium dimethyl, and
 17 dihalide complexes of the above. Di-alkyl, tri-alkyl,
 18 tetra-alkyl, and penta-alkyl cyclopentadienes, such as
 19 bis(pentamethylcyclopentadienyl)zirconium dimethyl, bis
 20 (1,2-dimethylcyclopentadienyl)zirconium dimethyl,
 21 bis(1,3-diethylcyclopentadienyl)zirconium dimethyl and dihalide
 22 complexes of the above. Silicone, phosphorus, and carbon
 23 bridged cyclopentadiene complexes such as
 24 dimethylsilyldicyclopentadienyl zirconium dimethyl or dihalide,
 25 methylphosphine dicyclopentadienyl zirconium dimethyl or
 26 dihalide, and methylene dicyclopentadienyl zirconium dimethyl
 27 or dihalide, carbenes represented by the formulae
 28 $\text{Cp}_2\text{Zr}=\text{CH}_2\text{P}(\text{C}_6\text{H}_5)_2\text{CH}_3$, and derivatives of these
 29 compounds such as $\text{Cp}_2\text{ZrCH}_2\text{CH}(\text{CH}_3)\text{CH}_2$.

30 Bis(cyclopentadienyl)hafnium dichloride,
 31 bis(cyclopentadienyl)hafnium dimethyl,
 32 bis(cyclopentadienyl)vanadium dichloride are illustrative of
 33 other metallocenes.

34 The ratio of aluminum in the alumoxane to total metal in
 35 the metallocenes can be in the range of 0.5:1 to
 36 10^5 :1, and preferably 5:1 to 10^3 :1. The molar
 37 ratio of zirconocene to titanocene can vary over a wide range

1 and in accordance with this invention the only limitation on
2 the molar ratios is the breadth of the MW distribution or the
3 degree of bimodality desired in the product polymer.

4 Desirably, the zirconocene to titanocene molar ratio will be
5 1:100 to 100:1, and preferably 1:10 to 1:1.

6 The solvents used in the preparation of the catalyst system
7 are inert hydrocarbons, in particular a hydrocarbon that is
8 inert with respect to the catalyst system. Such solvents are
9 well known and include, for example, butane, isobutane,
10 pentane, hexane, heptane, octane, cyclohexane,
11 methylcyclohexane, toluene, xylene and the like.

12 The catalyst systems described herein are suitable for the
13 polymerization of ethylene either in solution, slurry or gas
14 phase over a wide range of temperatures and pressures. For
15 example, such temperatures may be in the range of -60°C
16 to 280°C and especially in the range of 50°C to
17 160°C . The pressures employed in the process of the present
18 invention are those well known for, for example, in the range
19 of 1 to 500 atmospheres and even greater.

20 In a solution phase polymerization the alumoxane and
21 metallocene can be employed as a homogeneous catalyst system.
22 The alumoxane is preferably dissolved in a suitable solvent,
23 typically in inert hydrocarbon solvent such as toluene, xylene,
24 and the like in molar concentrations of 0.1M to 3M,
25 however, greater or lesser amounts can be employed.

26 The soluble metallocenes can be converted to supported
27 heterogeneous catalyst by depositing said metallocenes on
28 typical catalyst supports such as, for example, silica,
29 alumina, and polyethylene. The solid catalysts in combination
30 with an alumoxane can be usefully employed in slurry and gas
31 phase olefin polymerization.

32 After polymerization and deactivation of the catalyst, the
33 product polymer can be recovered by processes well known in the
34 art for removal of deactivated catalysts and solution. The
35 solvents may be flashed off from the polymer solution and the
36 obtained polymer extruded into water and cut into pellets or
37 other suitable comminuted shapes. Pigments, antioxidants and

1 other additives, as is known in the art, may be added to the
2 polymer.

3 The polymer product obtained in accordance with this
4 invention will have an average molecular weight in the range of
5 500 to 2,000,000 and preferably 10,000 to
6 500,000. The polymer will also have concentrations of average
7 molecular weights in the range of 500 to 100,000
8 and 100,000 to 1,000,000 for each sample.

9 The polymers produced by the process of this present
10 invention are capable of being fabricated into a wide variety
11 of articles, as is known for homopolymers of ethylene and
12 copolymers of ethylene and higher alpha-olefins. The present
13 invention is illustrated by the following examples.

14 In the examples following the molecular weights were
15 determined on a Water's Associates Model No. 150C GPC (Gel
16 Permeation Chromatography). The measurements were made by
17 dissolving polymer samples in hot trichlorobenzene (TCB) and
18 filtered. The GPC runs were performed at 145°C in TCB at 1.5
19 ml/min using two Shodex A80 M/S Gel columns of 9.4 mm internal
20 diameter from Perkin Elmer Inc. 300 milliliter of 3.1 percent
21 solutions in TCB were injected and the chromatographic runs
22 monitored at sensitivity equal -64 and scale factor equal 65.
23 The samples were run in duplicate. The integration parameters
24 were obtained with a Water's Associates data module. An
25 antioxidant, N-phenyl-2-naphthylamine, was added to all samples.

26 EXAMPLES

27 In the examples following the alumoxane was prepared in the
28 following manner:

29 600cc of a 14.5% solution of trimethylaluminum (TMA) in
30 heptane was added in 30cc increments at 5 minute intervals,
31 with rapid stirring, to 200cc toluene in a Zippoclave reactor
32 under nitrogen and maintained at 100°C. Each increment was
33 immediately followed by the addition of 0.3cc water. The
34 reactor was vented of methane after each addition. Upon

1 completion of the addition, the reactor was stirred for 6 hours
2 while maintaining the temperature at 100°C. The mixture,
3 contains soluble alumoxane and insoluble materials, is allowed
4 to cool to room temperature and settle. The clear solution
5 containing the soluble alumoxane is separated by decantation
6 from the solids.

7 Example 1

8 A 1-liter stainless steel pressure vessel, equipped with an
9 incline blade stirrer, an external water jacket for temperature
10 control, a septum inlet and vent line, and a regulated supply
11 of dry ethylene and nitrogen, was dried and deoxygenated with a
12 nitrogen flow. 500cc of dry, degassed toluene was introduced
13 directly into the pressure vessel. 20.0cc of alumoxane
14 solution (0.64 molar in total aluminum) was injected into the
15 vessel by a gas tight syringe through the septum inlet and the
16 mixture was stirred at 1,200 rpms and 50°C for 5 minutes at 0
17 psig of nitrogen. 0.091 mg bis(pentamethyl
18 cyclopentadienyl)zirconium dimethyl dissolved in 1.0 ml of dry,
19 distilled toluene was injected through the septum inlet into
20 the vessel followed by the injection of 0.906 mg
21 bis(cyclopentadienyl) titanium diphenyl in 10 ml of toluene.
22 After 1 minute, ethylene at 50 psig was admitted and while the
23 reaction vessel was maintained at 50°C. The ethylene was
24 passed into the vessel for 40 minutes at which time the
25 reaction was stopped by rapidly venting and cooling the
26 reactor. 20.1 gms of powdery white polyethylene having a \bar{M}_n of
27 58,600 and a \bar{M}_w of 323,000 with a molecular weight distribution
28 of 5.51. The GPC as shown in Fig. 1 showed a bimodal molecular
29 weight distribution.

30 Comparative Example 1A

31 Ethylene was polymerized under conditions identical to that
32 of Example 1 with the exception that the zirconocene only was
33 employed in combination with the alumoxane. 0.102 mg of the
34 zirconocene was employed. 20.6 gm of polyethylene was

1 obtained. The polyethylene had a \bar{M}_n of 42,000 and \bar{M}_w of
2 139,000 with a MWD of 3.31. The GPC as appears in Figure 3
3 evidenced a unimodal molecular weight distribution.

4 Comparative Example 1B

5 Ethylene was polymerized under conditions identical to that
6 of Example 1 with the exception that the titanocene only was
7 employed in combination with the alumoxane. 1.02 mg of the
8 titanocene was employed. 13.2gm of polyethylene was obtained.
9 The polyethylene had a \bar{M}_n of 184,000 and \bar{M}_w of 558,000 with a
10 MWD of 3.03. The GPC as appears in Figure 2 evidenced a
11 unimodal molecular weight distribution.

12 Example 2

13 A 1-liter stainless steel pressure vessel, equipped with an
14 incline blade stirrer, an external water jacket for temperature
15 control, a septum inlet and vent line, and a regulated supply
16 of dry ethylene and nitrogen, was dried and deoxygenated with a
17 nitrogen flow. 400cc of dry, degassed toluene was introduced
18 directly into the pressure vessel. 20.0cc of alumoxane (8
19 mmoles in total aluminum) was injected into the vessel by a gas
20 tight syringe through the septum inlet and the mixture was
21 stirred at 1,200 rpms and 80°C for 5 minutes at 0 psig of
22 nitrogen. 0.015 mg bis(cyclopentadienyl) zirconium dimethyl
23 dissolved in 1.0 ml of dry, distilled toluene was injected
24 through the septum inlet into the vessel followed by the
25 injection of 5.18 mg bis(cyclopentadienyl)titanium diphenyl in
26 10 ml of toluene. After 1 minute, ethylene at 60 psig was
27 admitted for 40 minutes while maintaining the reaction vessel
28 at 80°C. The reaction was stopped by rapidly venting and
29 cooling. 10.7 gms of powdery white polyethylene having a \bar{M}_n of
30 63,000 and a \bar{M}_w of 490,000 with a molecular weight distribution
31 of 7.8. The GPC as shown in Fig. 4 showed a bimodal molecular
32 weight distribution.

Example 3

A 1-liter stainless steel pressure vessel, equipped with an incline blade stirrer, an external water jacket for temperature control, a septum inlet and vent line, and a regulated supply of dry ethylene and nitrogen, was dried and deoxygenated with a nitrogen flow. 400cc of dry, degassed toluene was introduced directly into the pressure vessel. 20.0cc of alumoxane (8 mmols in total aluminum) was injected into the vessel by a gas tight syringe through the septum inlet and the mixture was stirred at 1,200 rpms and 50°C for 5 minutes at 0 psig of nitrogen. 0.151 mg bis(cyclopentadienyl) zirconium dimethyl dissolved in 1.0 ml of dry, distilled toluene was injected through the septum inlet into the vessel followed by the injection of 5.5 mg bis(cyclopentadienyl) titanium diphenyl in 10 ml of toluene. After 1 minute, ethylene at 60 psig was admitted for 40 minutes while maintaining the reaction vessel at 50°C. The reaction was stopped by rapidly venting and cooling. 13.8 gms of powdery white polyethylene having a \bar{M}_n of 16,500 and a \bar{M}_w of 89,000 with a molecular weight distribution of 5.4. The GPC as shown in Fig. 5 showed a bimodal molecular weight distribution.

Example 4

A 1-liter stainless steel pressure vessel, equipped with an incline blade stirrer, an external water jacket for temperature control, a septum inlet and vent line, and a regulated supply of dry ethylene and nitrogen, was dried and deoxygenated with a nitrogen flow. 400cc of dry, degassed toluene was introduced directly into the pressure vessel. 20.0cc of alumoxane (15 mmols in total aluminum) was injected into the vessel by a gas tight syringe through the septum inlet and the mixture was stirred at 1,200 rpms and 80°C for 5 minutes at 0 psig of nitrogen. 0.231 mg bis(cyclopentadienyl) zirconium dimethyl and 0.260 bis(ethylcyclopentadienyl)zirconium dimethyl, each dissolved in 1.0 ml of dry distilled toluene, were injected through the septum inlet into the vessel followed by the

1 injection of 0.535 mg bis(cyclopentadienyl)titanium diphenyl in
2 10 ml of toluene. After 1 minute, ethylene at 60 psig was
3 admitted for 40 minutes while maintaining the reaction vessel
4 at 80°C. The reaction was stopped by rapidly venting and
5 cooling. 24.0 gms of powdery white polyethylene having a \bar{M}_n of
6 43,000 and a \bar{M}_w of 191,000 with a molecular weight distribution
7 of 4.4.

8 Example 5

9 A 1-liter stainless steel pressure vessel, equipped with an
10 incline blade stirrer, an external water jacket for temperature
11 control, a septum inlet and vent line, and a regulated supply
12 of dry ethylene and nitrogen, was dried and deoxygenated with a
13 nitrogen flow. 400cc of dry, degassed toluene was introduced
14 directly into the pressure vessel. 20.0cc of alumoxane (15
15 mmoles in total aluminum) was injected into the vessel by a gas
16 tight syringe through the septum inlet and the mixture was
17 stirred at 1,200 rpm and 80°C for 5 minutes at 0 psig of
18 nitrogen. .201 mg bis(cyclopentadienyl)zirconium dimethyl and
19 0.216 mg bis(ethyl cyclopentadienyl)zirconium dimethyl each
20 dissolved in 1.0 ml of dry distilled toluene were injected
21 through the septum inlet into the vessel followed by the
22 injection of 0.506 mg bis(cyclopentadienyl) titanium diphenyl
23 in 10 ml of toluene. After 1 minute, ethylene at 50 psig was
24 admitted for 40 minutes while maintaining the reaction vessel
25 at 80°C. The reaction was stopped by rapidly venting and
26 cooling. 25.2 gms of powdery white polyethylene having a \bar{M}_n of
27 39,700 and a \bar{M}_w of 168,000 with a molecular weight distribution
28 of 4.2 and bimodal \bar{M}_w distribution.

29 Example 6

30 A 1-liter stainless steel pressure vessel, equipped with an
31 incline blade stirrer, an external water jacket for temperature
32 control, a septum inlet and vent line, and a regulated supply
33 of dry ethylene and nitrogen, was dried and deoxygenated with a
34 nitrogen flow. 500cc of dry, degassed toluene was introduced

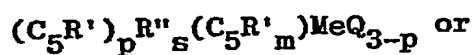
1 directly into the pressure vessel. 10.0cc of alumoxane (8
2 moles total aluminum) was injected into the vessel by a gas
3 tight syringe through the septum inlet and the mixture was
4 stirred at 1,200 rpms and 80°C for 5 minutes at 0 psig of
5 nitrogen. 0.260 mg bis(cyclopentadienyl)zirconium dimethyl and
6 0.204 mg bis(ethyl cyclopentadienyl)zirconium dimethyl each
7 dissolved in 1.0 ml of dry distilled toluene were injected
8 through the septum inlet into the vessel. After 1 minute,
9 ethylene at 60 psig was admitted for 12 minutes while
10 maintaining the reaction vessel at 80°C. The reaction was
11 stopped by rapidly venting and cooling. 32.0 gms of powdery
12 white polyethylene having a \bar{M}_n of 47,100 and a \bar{M}_w of 183,000
13 with a molecular weight distribution of 3.9.

CLAIMS:

1. A catalyst system for the (co)polymerization of ethylene to polyethylene having a broad molecular weight distribution, said catalyst comprising (a) at least two different metallocenes which are mono, di or tricyclopentadienyl derivatives of a Group 4b, 5b and 6b transition metal each having different propagation and termination rate constants for ethylene polymerizations and (b) an alumoxane.

2. A catalyst system for the (co)polymerization of ethylene to polyethylene having a broad and/or multimodal molecular weight distribution; said catalyst comprising:

(a) at least two or more metallocenes represented by the general formula



$R''_s (C_5R'_m)_m MeQ'$, each having a different propagation and termination rate constant, and

(b) an alumoxane

wherein $(C_5R'_m)_m$ is a cyclopentadienyl or substituted cyclopentadienyl, each R' which can be the same or different is hydrogen or a hydrocarbyl radical or two R' substituents together form a fused C_4-C_6 ring, R'' is a C_1-C_4 alkylene radical, a dialkyl germanium or silicone or alkyl phosphine or amine radical bridging two $(C_5R'_m)_m$ rings, each Q , which may be the same or different, is a hydrocarbon radical or halogen, Q' is an alkylidene radical having from 1 to 20 carbon atoms, Me is a Group 4b, 5b or 6b metal, s is 0 or 1, p is 0, 1 or 2; when p is 0, s is 0; m is 4 when s is 1; and m is 5 when s is 0.

3. The catalyst system of claim 2 comprising two zirconocenes.

4. The catalyst system of claim 2 comprising two titanocenes.

5. The catalyst system of claim 3 comprising at least 2 zirconocenes and 1 titanocene.

6. The homogeneous catalyst system of claim 4 comprising at least 2 titanocenes and 1 zirconocene.

7. A process for producing polyethylene having a broad and/or multimodal molecular weight distribution comprising polymerizing ethylene in the presence of the catalyst system as claimed in any of claims 1 to 6.

8. Polyethylene having a broad and/or multimodal MWD obtained by polymerizing ethylene in the presence of a catalyst system as claimed in any of claims 1 to 6.

9. The polyethylene of claim 8 having a bimodal MWD.

10. The polyethylene of claim 9 wherein the Mw/Mn ratio is in the range of 2 to 50.

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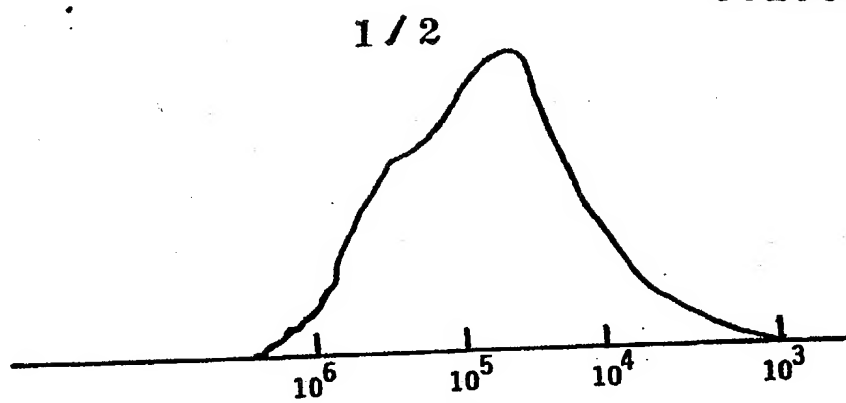


FIG. 1

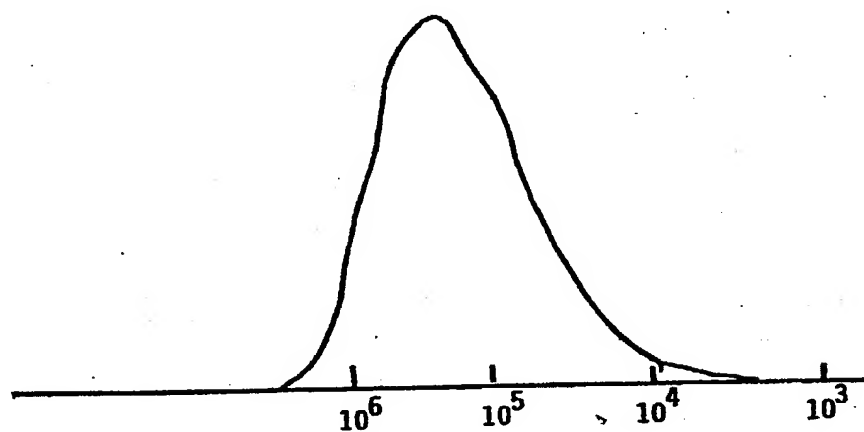


FIG. 2

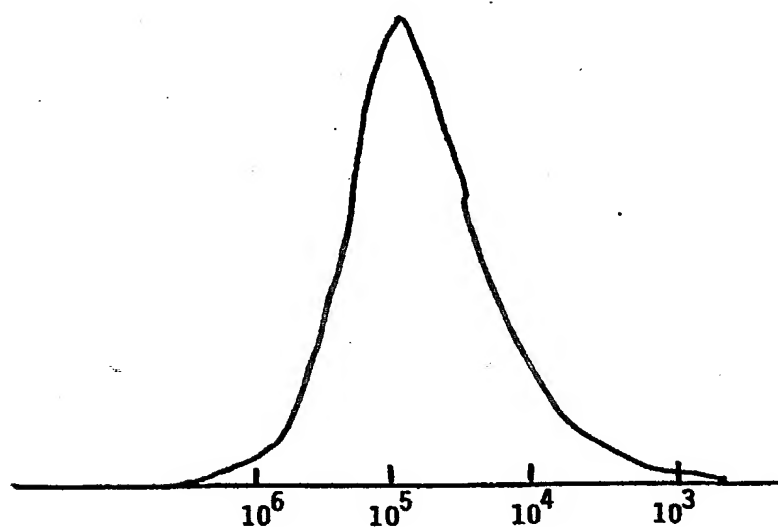


FIG. 3

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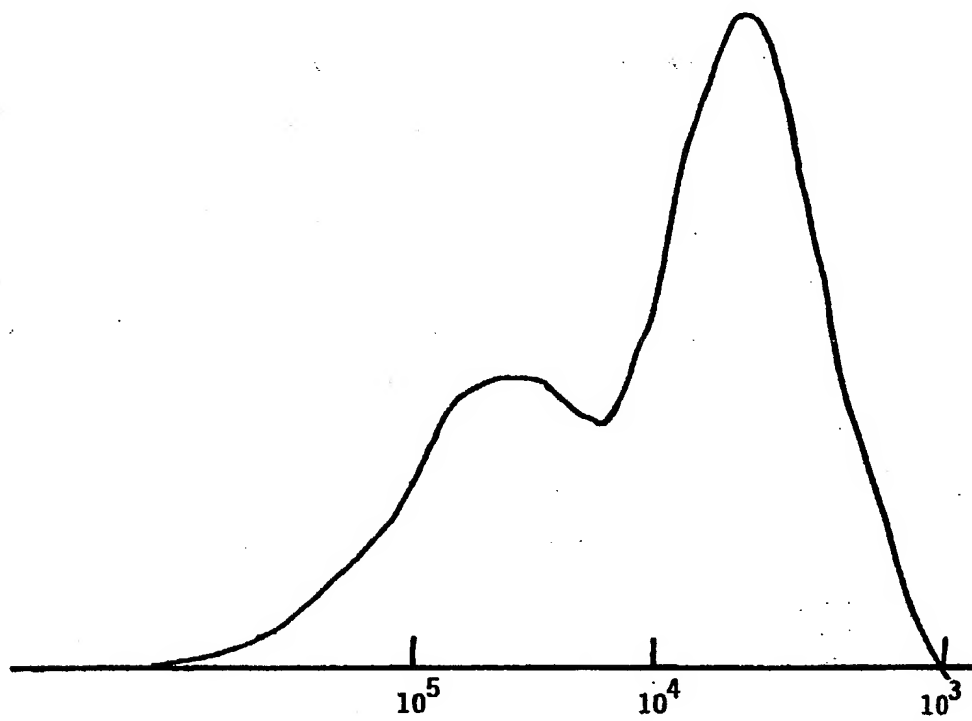


FIG. 4

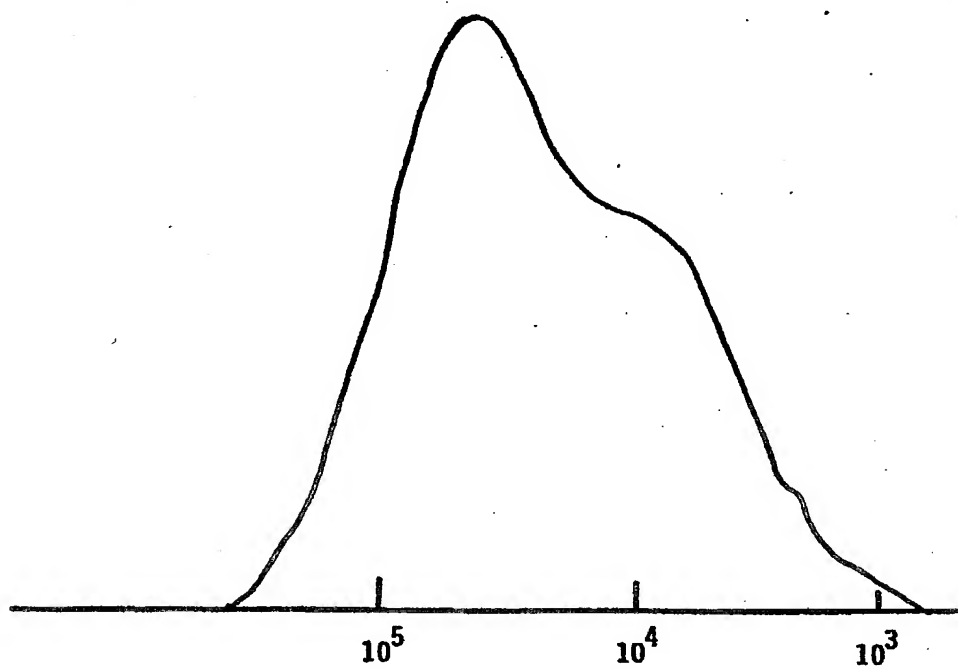


FIG. 5



European Patent
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EUROPEAN SEARCH REPORT

0128045

Application number

EP 84 30 3804

DOCUMENTS CONSIDERED TO BE RELEVANT			
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int. Cl. 7)
A	EP-A-0 069 951 (HOECHST) * Claims 1-8 *	1	C 08 F 10/00 C 08 F 4/62
D, A	EP-A-0 035 242 (HANSJÖRG SINN) * Claims 1-2 *	1	
A	GB-A-1 233 599 (MONSANTO) * Page 1, line 61 - page 2, line 17 *	1	
			TECHNICAL FIELDS SEARCHED (Int. Cl. 7)
			C 08 F
The present search report has been drawn up for all claims			
Place of search THE HAGUE		Date of completion of the search 13-09-1984	Examiner WEBER H.
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